## OVERALL Average = 130 SD = 40

## UNIVERSITY OF CALIFORNIA, BERKELEY

MECHANICAL ENGINEERING ME106 Fluid Mechanics

1st Test, S19 Prof S. Morris

NAME \_\_\_\_\_

1. (100) In a certain plane flow, the fluid velocity  $\mathbf{V} = v_x \mathbf{i} + v_y \mathbf{j}$  is given by

$$v_x = kyx^2, \quad v_y = -kxy^2, \tag{1.1}$$

where k > 0 is constant.

- **10** (a) Show that (1.1) satisfies the no-slip condition on x = 0, and also on y = 0.
- **30** (b) Find, and sketch, the streamlines.
- **30** (c) Calculate the components  $a_x$  and  $a_y$  of the fluid acceleration. On your sketch in part (b), show the position vector  $\mathbf{r}$  and the fluid acceleration  $\mathbf{a}$ .
- **30** (d) In an arbitrary flow of a Newtonian fluid, the shear stress  $\tau$  exerted by the fluid in the *x*-direction on a surface whose normal is in the Oy direction is given by

$$\tau = \mu \Big( \frac{\partial v_x}{\partial y} + \frac{\partial v_y}{\partial x} \Big). \tag{1.2}$$

Average = 75 SD = 20

Using (1.2), find the x-component of force exerted by the flow (1.1) on the length 0 < x < L of the upper side of the boundary y = 0. Show that your result is dimensionally correct.\*

Solution

(a) At 
$$x = 0$$
,  $v_y = 0$ ; at  $y = 0$ ,  $v_x = 0$ 

(b)

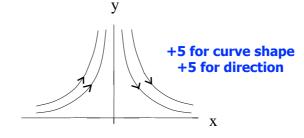
+5 ge	enera	l eq	n, +5 p	lug in V
$\mathrm{d}x$	$\mathrm{d}y$		$\mathrm{d}x$	$\mathrm{d}y$
$\overline{v_x}$ =	$\overline{v_u}$	$\Rightarrow$	$\overline{kyx^2} =$	$=-\frac{1}{kxy^2}$ .

By cancelling a common factor of kxy,

## +10 simplify and solve

$$\frac{\mathrm{d}x}{x} = -\frac{\mathrm{d}y}{y} \; \Rightarrow \; y\mathrm{d}x + x\mathrm{d}y = 0 \; \Rightarrow \; \mathrm{d}(xy) = 0$$

Streamlines are rectangular hyperpolae xy = const.



<sup>\*</sup> Because this is a plane flow, your answer will have dimensions of force per unit length.

(c) <u>Method 1.</u> Direct calculation, using definition of fluid acceleration at point  $\{x, y\}$  as the acceleration of the fluid particle currently at that point. (See point allocation for Method 2)

Let X(t), Y(t) be the coordinates of a fluid particle. The velocity of this particle is, by (1.1).

$$\dot{X} = kYX^2, \ \dot{Y} = -kXY^2.$$
 (1.3*a*, *b*)

Its acceleration has the x-component

$$\ddot{X}(t) = k\{2XY\dot{X} + X^{2}\dot{Y}\}, = k^{2}\{2X^{3}Y^{2} - X^{3}Y^{2}\}, = k^{2}X^{3}Y^{2}.$$
(1.4*a*, *b*, *c*)

Eq.(1.4a) follows by using the product rule; (1.4b) follows from (1.4a) by substituting for  $\dot{X}$ ,  $\dot{Y}$ . The *y*-component is

$$\ddot{Y}(t) = -k\{\dot{X}Y^2 + 2XY\dot{Y}\}, = -k^2\{X^2Y^3 - 2X^2Y^3, = k^2X^2Y^3.$$
(1.5*a*, *b*, *c*)

The acceleration of the particle is :

$$\mathbf{a} = k^2 X^2 Y^2 \{ \mathbf{i} X + \mathbf{j} Y \} : \tag{1.6}$$

at point  $X\mathbf{i} + Y\mathbf{j}$ . Because this holds for all X and Y, the acceleration is given in the spatial description by

$$\mathbf{a}(x,t) = k^2 x^2 y^2 \{\mathbf{i}x + \mathbf{j}y\}$$

Method 2. Equivalent procedure, expressed in terms of the material derivative.

$$\mathbf{a} = \frac{\mathrm{d}\mathbf{V}}{\mathrm{d}t} = \frac{\partial\mathbf{V}}{\partial t} + (\mathbf{V}\cdot\nabla)\mathbf{V}, \qquad \mathbf{+5 \text{ general equation}}$$
$$= \frac{\partial\mathbf{V}}{\partial t} + v_x\frac{\partial\mathbf{V}}{\partial x} + v_y\frac{\partial\mathbf{V}}{\partial y} + v_z\frac{\partial\mathbf{V}}{\partial z} + \mathbf{10 \text{ expanded convective term}}$$
$$= 0 + kyx^2\frac{\partial\mathbf{V}}{\partial x} - kxy^2\frac{\partial\mathbf{V}}{\partial y}$$
$$= kyx^2\{2kxy\mathbf{i} - ky^2\mathbf{j}\} - kxy^2\{kx^2\mathbf{i} - 2kxy\mathbf{j}\}$$
$$= k^2\{x^3y^2\mathbf{i} + x^2y^3\mathbf{j}\}, \qquad \mathbf{+5 \text{ correct answer}}$$

as by method 1.

On y = 0

<u>Sketch.</u> Must show that  $\mathbf{a} \parallel \mathbf{r}$ . **+10** 

(d) For the flow (1.1)

$$\frac{\partial v_x}{\partial y} = kx^2, \ \frac{\partial v_y}{\partial x} = -ky^2$$

$$\tau = \mu k x^2$$
. +10 shear (+5/10 is not evaluated at y=0)

Resultant force in x-direction on strip 0 < x < L:

$$F_x = \int_0^L \tau \, \mathrm{d}x = \frac{1}{3} \mu k L^3 \qquad \textbf{+10 force}$$

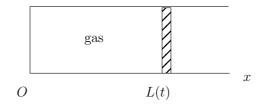
Dimensions:  $[k] = L^{-2}T^{-1}$  (from expression for **V**),  $[\mu] = ML^{-1}T^{-1} \Rightarrow [\mu kL^3] = MT^{-2} = [F/L]$ . dimensionally consistent. +10 dimensions

1S19-2

## Average = 60 SD = 30

**2.** (100) A fixed mass of gas is compressed by pushing the piston inwards: the length L(t) of the gas column decreases with time. The flow is one-dimensional with acceleration  $\mathbf{a} = a_x \mathbf{i}$ ;  $a_x = \dot{L} x/L$ . where  $\ddot{L} = d^2 L/dt^2$ . Because  $a_x \neq 0$ , the Euler equation  $\rho a_x = -\frac{\partial p}{\partial x}$  (negligible gravity) requires there to be a pressure gradient. As a result, the density  $\rho$  varies in x from its value  $\rho_0(t)$  at x = 0 to  $\rho_L(t)$  at x = L.

- **40** (a) If  $|\rho_L \rho_0| \ll \rho_0$ , density can, to a first approximation, be taken as uniform in x. Assuming this to be so, find p(x,t) as a function of  $p_0(t) = p(0,t)$ ,  $\rho_0(t)$ ,  $\ddot{L}$ , L and x. Show that your answer is dimensionally correct.
- **50** (b) Using the result of part (a), and Taylor's theorem, find  $\rho_L \rho_0$  as a function of  $\rho_0$ , L,  $\ddot{L}$  and the (isentropic) bulk modulus.  $K_S = \rho \left(\frac{\partial p}{\partial \rho}\right)_S$ .
- 10 (c) Estimate  $(\rho_L \rho_0)/\rho_0$  for a car engine idling with angular velocity  $\omega = 10^2$  rad/s,  $\rho_0 = 1$  kg/m<sup>3</sup>,  $K_S = 10^5$  Pa when L = 0.1 m: assume that  $\ddot{L} = \omega^2 L$ .



Solution

(a) Euler equation: 
$$\frac{\partial p}{\partial x} = -\rho(0,t)\frac{L}{L}x$$
,  
 $\Rightarrow p(x,t) = p(0,t) - \rho(0,t)\frac{\ddot{L}}{2L}x^2$ 
+30 plug in for a\_x  
integrate  
evaluate at bounds  
constant of p(0,t) (2.1)

Dimensions

L.H.S. : 
$$[p] = FL^{-2} = ML^{-1}T^{-2}$$
.  
R.H.S. :  $[\rho Lx^2/L] = ML^{-3}L^3T^{-2}L^{-1}$ ,  $= ML^{-1}T^{-2}$ . Consistent.  
(b) Taylor's theorem:  
 $\rho(L,t) = \rho(0,t) + \{p_L(t) - p_0(t)\} \left(\frac{\partial p}{\partial \rho}\right)_S \Big|_0 + h.o.t.$   
 $\Rightarrow \frac{\rho_L - \rho_0}{\rho_0} = \frac{p_L - p_0}{(K_S)_0}$ . +20 (2.3)

By substituting into (2.3) the result of evaluating (2.1) at x = L,

$$\frac{\rho_L - \rho_0}{\rho_0} = -\rho_0 \frac{L\ddot{L}}{2(K_S)_0}.$$
 +20 plug in and evaluate (2.4)

(c) For the numbers given,

$$\left|\frac{\rho_L - \rho_0}{\rho_0}\right| = \rho_0 \omega^2 \frac{L^2}{2(K_S)_0}, = 5 \times 10^{-4}.$$
 +10

1S19 - 3