Midterm II

(Closed Book and notes, two 8.5"x11" sheet of notes is allowed)

Printed Name _____

By signing this sheet, you agree to adhere to the U.C. Berkeley Honor Code

Signed Name_____

	1)/10
	2)/10
	3)/10
	4)/20
	5)/30
Total:	/80

- 1. (10 Pts.) The rate law for the irreversible reaction $A \rightarrow B + C$ is known to be as follows: $r_A = -k/C_A$. In an experiment, the concentration of A was monitored as a function of time in a constant volume BSTR.
 - a) Which technique would you use to find the rate constant, k? (4 pts.)
 - b) How would you find the value of k graphically? (6 pts.)

2. (10 Pts.) The irreversible gas-phase reaction of SO_2 to SO_3 is to be carried out in a PFR at a pressure of 10 atm. The inlet feed includes a 50-fold stoichiometric excess of O_2 to assure complete conversion of SO_2 . The inlet flow rate is 50 m³/min and the temperature is 800K.

$$SO_2 + \frac{1}{2} O_2 \rightarrow SO_3$$

a) You are given data on the partial pressure of product, p_{SO_3} , along the length of the reactor. How would you plot this data to obtain the reaction order with respect to SO₂? Be specific as to exactly what you would plot and how you would plot it. (6 pts.)

b) How would you propose to determine the reaction order with respect to O_2 ? Would this require additional data, and if so, what data would be needed? (4 pts.)

3. (10 Pts) A hydrogen stream to a fuel cell must be cleaned up of any CO, since CO will poison the catalyst. The removal of CO can be done with a catalyst that combusts CO selectively in the presence of H₂. The kinetics for the two reactions are given by:

1. $\rm CO + 1/2O_2 \rightarrow CO_2$	$r_1 = k_1 P_{O2} / P_{CO}$	$k_1 = k_1^{o} exp(-E_1/RT)$
2. $H_2 + 1/2O_2 \rightarrow H_2O$	$r_2 = k_2 P_{\rm O2} P_{\rm H2}$	$k_2 = k_2^{o} exp(-E_2/RT)$
$E_1 > E_2$		

a) What type of reactor should be used to maximize the combustion of CO relative to H_2 ? Please be sure to explain your answer.

b) Should the reactor of your choice be run at high or low temperature? Be sure to explain your answer.

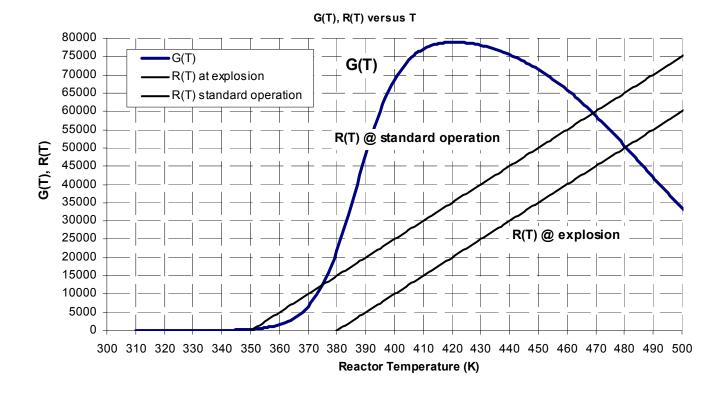
- 4. (20 Pts.) Consider a first-order gas-phase reaction occurring in a PFR. The reactor is jacketed so that heat can be added or removed through the walls of the reactor. The heat flux through the wall per unit volume of reactor is given by q = Ua(Ta-T).
 - a) Assume the reaction is exothermic and reversible. On the same graph, sketch the temperature profile (T versus V) for the following two cases: 1) adiabatic operation, 2) non-adiabatic operation and $T_a < T_o$. Label T_a and T_o on your graph.

b) On a separate graph, sketch the optimal temperature profile to maximize the conversion. Assume the maximum operating temperature is T_m .

5. (30 Pts.) The liquid phase reaction of J ↔ Z takes place in a superheated steam jacketed CSTR with pure J as the feed. An operator in charge of monitoring the reactor decides that everything is quiet and steps out to have a quick cup of coffee. While away, a loud explosion is heard coming from the direction of the CSTR. The operator runs back and finds that the CSTR has exploded. In the follow-up investigation, the reactor was found to have heated up to above the reactor design specifications. The shaken operator explained that the reactor was definitely operating below 370 K when she left.

<u>The last readings on operator's clipboard:</u> Inlet feed temperature = 305K Temperature of the heated jacket = 355K Molar flowrate of feed = 10 mol/min

 $\frac{\text{Reactor Specifications:}}{\text{E/R} = 20,000 \text{ K}}$ $C_{pJ} = 50 \text{ cal/mol·K}$ $C_{pZ} = 20 \text{ cal/mol·K}$ $U \cdot A = 4500 \text{ cal/min·K}$ $\Delta H_{rxn} = -83,000 \text{ cal/mol·K}$ volumetric flowrate = 20 dm³/min



a) Approximately what was the temperature of the reactor when the operator left for coffee? Use plot shown above.

- b) Could the reactor operate at another temperature(s) under the conditions when the operator left? If so, at what temperature(s)? Show work.
- c) Which temperature(s) are most likely to occur? (i.e., stable)
- d) The investigators found that the control mechanism for the superheated steam jacket was jammed open and the final reactor temperature (assumed at steady state) before the CSTR exploded was 480K. What was the temperature of the heated jacket when the reactor exploded? Show calculation.

e) What was the conversion right before the reaction exploded?