

+

Prob. 1

$$\Delta P = RQ$$

Hagen - Poiseuille ~~eff~~

$$Q = \frac{\pi}{128 \mu} \frac{\Delta P}{L} D^4$$

a)

$$\frac{\Delta P}{Q} = R = \frac{128 \mu L}{\pi D^4}$$

(5)

Tube 1.

$$R_1 = \frac{128 \mu}{\pi} \left(\frac{L_1}{D_1^4} + \frac{L_2}{D_2^4} \right)$$

Tube 2.

$$R_2 = \frac{128 \mu (L_1 + L_2)}{D_1^4}$$

a. know ΔP find Q

$$Q_1 = \frac{\Delta P}{R_1} = \frac{\Delta P \cdot \pi}{128 \mu} \left(\frac{L_1}{D_1^4} + \frac{L_2}{D_2^4} \right)$$

$$= \frac{\Delta P \cdot \pi \cdot D_1^4 D_2^4}{128 \mu (L_1 D_2^4 + L_2 D_1^4)} \quad (5)$$

$$Q_2 = \frac{\Delta P}{R_2} = \frac{\Delta P \cdot \pi \cdot D_1^4}{128 \mu (L_1 + L_2)}$$

$$Q_2 > Q_1 \Rightarrow \frac{Q_1}{Q_2} < 1$$

$$\frac{Q_1}{Q_2} = \frac{\Delta P \cdot \pi}{128 \mu} \frac{D_1^4 D_2^4}{(L_1 D_2^4 + L_2 D_1^4)} \cdot \frac{128 \mu (L_1 + L_2)}{\Delta P \cdot \pi \cdot D_1^4}$$

$$= \frac{D_1^4 D_2^4 (L_1 + L_2)}{D_1^4 (L_1 D_2^4 + L_2 D_1^4)}$$

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+ Prob. 1

$$\text{if } L_2 = 0 \Rightarrow \frac{Q_1}{Q_2} = 1 \text{ makes sense}$$

$$\text{if } L_1 = 0 \Rightarrow \frac{Q_1}{Q_2} = \frac{D_2^4 L_2}{D_1^4 L_2} = \frac{D_2^4}{D_1^4}$$

$$\text{know } D_2 < D_1 \Rightarrow \frac{Q_1}{Q_2} \leq 1$$

(P)
(5)

b. given ΔP which tube has a higher V_{max}

$$V_{max} \approx \bar{V}$$

$$\bar{V} = \frac{4Q}{\pi D^2}$$

$$\begin{aligned} \bar{V}_1 &= \frac{4Q_1}{\pi D_2^2} = \frac{4}{\pi D_2^2} \frac{\Delta P \pi}{128 \mu} \frac{D_1^4 D_2^4}{(L_1 D_2^4 + L_2 D_1^4)} \\ &= \frac{\Delta P}{32 \mu} \frac{D_1^4 D_2^2}{(L_1 D_2^4 + L_2 D_1^4)} \end{aligned} \quad (5)$$

$$\bar{V}_2 = \frac{4Q_2}{\pi D_1^2} = \frac{\Delta P}{32 \mu} \frac{D_1^2}{(L_1 + L_2)}$$

as $L_2 \rightarrow 0$

$$\bar{V}_1 = \frac{\Delta P}{32 \mu} \frac{D_1^4 D_2^2}{L_1 D_2^4} = \frac{\Delta P}{32 \mu} \frac{1}{L_1} \frac{D_1^4 D_2}{D_2^2}$$

$$\bar{V}_2 = \frac{\Delta P}{32 \mu} \frac{D_1^2}{L_1}$$

$$\frac{\bar{V}_1}{\bar{V}_2} = \frac{D_1^4}{D_2^2} \frac{1}{D_1^2} = \frac{D_1^2}{D_2^2} > 1$$

(5)

$D_2 < D_1$

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i) if $L_1 \rightarrow 0$

$$\bar{V}_1 = \frac{\Delta P}{32\mu} \frac{D_1^4 D_2^4}{L_2 D_1^4} = \frac{\Delta P}{32\mu L_2} \frac{1}{D_2^2}$$

$$\bar{V}_2 = \frac{\Delta P}{32\mu} \frac{D_1^2}{L_2}$$

$$\frac{\bar{V}_1}{\bar{V}_2} = \frac{D_2^2}{D_1^2} \quad D_2 < D_1$$

$$\frac{\bar{V}_1}{\bar{V}_2} < 1 \quad \text{At some } L_1 \neq L_2 \\ \bar{V}_1 = \bar{V}_2$$

$$1 = \frac{D_1^4 D_2^2}{L_1 D_2^4 + L_2 D_1^4} \cdot \frac{(L_1 + L_2)}{D_1^2}$$

$$= \frac{D_1^2 D_2^2 (L_1 + L_2)}{L_1 D_2^4 + L_2 D_1^4}$$

There are multiple
sols for
various D_1 & D_2

⑤

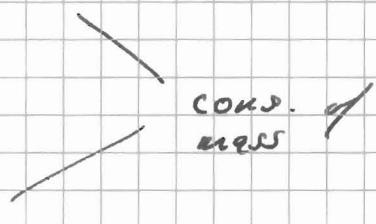
c. if Q is fixed

$\Rightarrow Q_1 = Q_2$ so they both have the same
flow rate

⑥

d. Tube 1 has a higher V_{max}

by a factor $\frac{D_1^2}{D_2^2}$



pressure $\Rightarrow Q_2 > Q_1$

V_{max1} & V_{max2} are not
unique

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Hi Dorian!

So the shortest cut for problem 1 b) a. is knowing that $\bar{u}_z = \frac{1}{2}u_{z\max}$. This can be derived as follows:

The reduces NV-equation for the round pipe case on polar cylinder coordinates is:

$$\frac{1}{r} \frac{\partial}{\partial r} \left(r \frac{\partial u_z}{\partial r} \right) = \frac{1}{\mu} \frac{\partial p}{\partial z}$$

The solution (integrate twice) of which is given by: $u_z = \frac{1}{4\mu} \frac{\partial p}{\partial z} r^2 + c_1 \ln r + c_2$

Since at $r = 0$ (middle of the tube) the velocity cannot diverge $c_1 = 0$. The no-slip boundary conditions

at $r = R$ (pipe wall) lead to $c_2 = -\frac{1}{4\mu} \frac{\partial p}{\partial z} R^2$.

$$\Rightarrow u_z = -\frac{1}{4\mu} \frac{\partial p}{\partial z} (R^2 - r^2)$$

The velocity is obviously highest in the middle at $r = 0$: $u_{z\max} = -\frac{1}{4\mu} \frac{\partial p}{\partial z} R^2$

The average velocity can be simply obtained by integration over the pipe radius and dividing by the cross-sectional area of the pipe:

$$\bar{u}_z = \frac{1}{\pi R^2} \int_0^R u_z \cdot 2\pi r dr = \frac{1}{\pi R^2} \int_0^R \left[-\frac{1}{4\mu} \frac{\partial p}{\partial z} (R^2 - r^2) \right] 2\pi r dr = \frac{1}{2} \left[-\frac{1}{4\mu} \frac{\partial p}{\partial z} R^2 \right] = \frac{u_{z\max}}{2}.$$

Many students remembered actually from their basic fluid mechanics course that $\bar{u}_z = \frac{1}{2}u_{z\max}$... This

makes the problem really simple since $\bar{u}_z = \frac{Q}{\pi R^2}$ where Q is given by $Q = \frac{\Delta P}{R}$ from Ohm's law of fluid mechanics (an expression R was to be derived in 1a) from Hagen-Poiseuille equation).

Combine all this and you'll get: $u_{z\max} = 2 \cdot \frac{1}{R} \cdot \frac{1}{\pi R^2} \cdot \Delta P$

Thus, deciding in which tube the maximum exit velocity is higher comes down to evaluating for which tube the product of the above expression is larger as a function of parameters. Please note:

- For the simple tube an expression for \mathcal{R} is just the result of 1a).
- One has to treat the composite tube simply as two resistors in series by analogy to electronics.
- When evaluating $u_{z_{\text{exit}}}$ using the above expression for the simple tube ΔP is just the “given pressure drop”. For the composite tube one has to use the pressure drop across the second segment *only*. This pressure drop can be calculated from the pressure drop across the entire system by using the “voltage divider rule” by analogy to electronics: $\Delta P_2 = \frac{\mathcal{R}_2}{\mathcal{R}_1 + \mathcal{R}_2} \cdot$

+ problem 3

params

$$u \text{ (m/s)}$$

$$h \text{ (m)}$$

$$l \text{ (m)}$$

$$\delta \text{ (m²/s)}$$

2 units m/s

\Rightarrow 2 TT groups (5)

$$TT_1 = \frac{u \text{ (m/s)}}{\delta \text{ (m²/s)}} h \text{ (m)} = \frac{uh}{\delta} \quad (5)$$

$$TT_2 = \frac{h}{l} \quad (5)$$

$$\frac{uh}{\delta} = g\left(\frac{h}{l}\right) \quad (5)$$

$$= f\left(\frac{l}{h}\right)$$

assume f is linear $\Rightarrow l$ increases u increases (5)

$$\frac{uh}{\delta} = c \frac{l}{h}$$

$u = c \frac{l \delta}{h^2}$

(5)